

ACTIVITY COEFFICIENTS OF AQUEOUS SOLUTIONS OF NaOH AND KOH IN WIDE CONCENTRATION AND TEMPERATURE RANGES

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Up to now, there exist a quite wide temperature interval between 70 or 80 and 150 °C with no sufficiently reliable experimental data of mean activity coefficients for aqueous NaOH as well as KOH solutions. In order to fill this gap, it was tried to derive suitable correlation equations for this quantity in dependence on the molality (for NaOH in the range $m_{\text{NaOH}} = 2\text{--}25 \text{ mol kg}^{-1}$, for KOH in the range $m_{\text{KOH}} = 2\text{--}18 \text{ mol kg}^{-1}$) and temperature (in the range 0–200 °C for both kinds of solutions) on the basis of the available data of this quantity and with the use of the previously derived correlation equations for the water activity in aqueous solutions of NaOH and KOH under the same conditions. The comparison between the calculated and experimental data was discussed.

Key words: Mean activity coefficient; Aqueous solutions; NaOH; KOH.

For the thermodynamic calculation of the equilibrium states of chemical or electrochemical reactions with the participation of aqueous solutions of NaOH or KOH it is necessary to know their activities under real reaction conditions. The activity of a 1 : 1 electrolyte is usually expressed by the product of its total molality and the appropriate practical mean activity coefficient at the given molality and temperature, i.e. $a_{\text{MeOH}} = (m_{\text{MeOH}} \gamma_{\pm\text{MeOH}})^2$. The quantitative concentration and temperature dependence of the mean activity coefficients of aqueous solutions of strong electrolytes, based on the Debye–Hückel theory^{1–5}, is mostly complicated. Some methods of theoretical calculations of activity coefficients (e.g. according to Pitzer⁶, Bromley^{7,8} or Messner⁹) give sufficiently reliable results for a limited range of concentrations only, e.g. for NaOH or KOH solutions in the range of 0–6 mol kg⁻¹ (ref.¹⁰). For various technical processes, however, even more concentrated solutions of sodium or potassium hydroxides are frequently used at temperatures less or more different from the reference temperature of 25 °C. Until now, however, the overall relations for the mean practical activity coefficients of aqueous solutions of NaOH or KOH valid in a necessary wide range of their molality as well as temperature are not available.

A critical evaluation of the all published sufficiently reliable data of the mean practical coefficients of aqueous solutions of NaOH and KOH at 25 °C was presented by Hammer and Wu in 1972 (ref.¹¹). The smoothed data were fitted with the aid of an extended Debye–Hückel equation

$$\log \gamma_{\pm} = -A_{\gamma} |z_+ z_-| I^{0.5} / (1 + BI^{0.5}) + \beta I + CI^2 + DI^3 + \dots, \quad (1)$$

where I stands for the ionic strength defined by the relation

$$I = 0.5 \sum_{i=1}^k m_i z_i^2. \quad (2)$$

B , β , C and D denote the specific constants for the given electrolyte at the given temperature, z_+ and z_- are the charge numbers of the appropriate cation and anion, and A_{γ} represents the temperature dependent value of the Pitzer–Debye–Hückel limiting slope for the activity coefficients in aqueous solutions (e.g. $A_{\gamma} = 0.51084$ at 25 °C (ref.¹¹)). It must, however, be mentioned that the value of this quantity changed a little as time went due to the progressive precision of the dielectric constant of water; its recent internationally recognized values may be calculated from the values of the limiting slopes for the osmotic coefficients, A_{ϕ} , for the range of 0–350 °C and from saturation to 1 kbar (ref.¹²), using the relation $A_{\gamma} = 3A_{\phi}$.

The mean activity coefficients of aqueous solutions of sodium and potassium hydroxides in dependence on their concentration and temperature were also determined several times. Harned and Hecker¹³ measured these values for 0.05–4.0 M NaOH at 0–35 °C. Similar measurements for KOH solutions were published by Harned and Cook¹⁴. Analogous measurements for NaOH solutions at wider concentration as well as temperature ranges (i.e. 0.1–17 mol kg⁻¹) were done by Akerlöf and Kegeles¹⁵ and for KOH solutions by Akerlöf and Bender¹⁶. Zarembo et al.¹⁷ published the data of the mean activity coefficients of 0.85–23.8 M NaOH and 0.85–17.5 M KOH solutions at 423–623 K (i.e. 150–350 °C) in intervals of 50 K. Further data for 1–8 M NaOH and KOH as well as for 1–5 M LiOH solutions at –10 to 120 °C were presented by Pound et al.¹⁸ in 1986. These data, however, exhibit an unusual course of the temperature dependence in the range of –10 to 40 °C for NaOH solutions and –10 to 60 °C for KOH solutions. Further, the numerical values of the activity coefficients at 60–80 °C differ considerably from the values for the solutions of the same composition referred by other authors^{2,3,13–16}, although their temperature trend is similar (see Figs 1 and 2). Moreover, values of $\gamma_{\pm, \text{KOH}}$ instead of $\log \gamma_{\pm, \text{KOH}}$ are most probably given for 263 K in Table 6 of ref.¹⁸. Therefore, neglecting the data of Pound et al.¹⁸ as insufficiently reliable, it may be concluded that there exists a quite wide interval between 70–150 °C and 80–150 °C for NaOH and KOH solutions, respectively, with no sufficiently reliable values of the mean activity coefficients. It is, however, evident that a simple extrapolation of existing data into this temperature range is hardly possible, especially for lower solution concentrations. Only for NaOH solutions, it seems to be possible to

extrapolate high temperature data for 20–24 M NaOH (ref.¹⁷) till down to 25 °C where they coincide with the smoothed NBS data¹¹ at this temperature. Therefore, in order to gain sufficiently reliable data of the mean activity coefficients of NaOH and KOH solutions in the whole wanted range of molalities and temperatures, it is necessary either to undertake new experimental measurements or to try to correlate all till available experimental data in a proper way for the whole range of molalities and temperatures as well. It must, however, be taken into account that such a correlation can lead to an expression with a lower reliability grade. The latter method presents the subject of this communication.

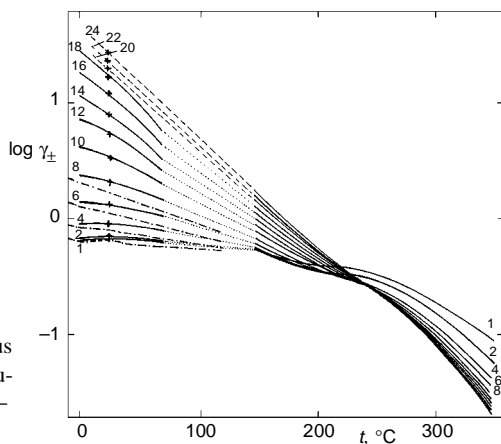


FIG. 1

Temperature dependence of $\log \gamma_{\pm}$ for various molalities of aqueous sodium hydroxide solutions: + (ref.¹¹), — (refs.^{15,17}), - - - (ref.¹⁸)

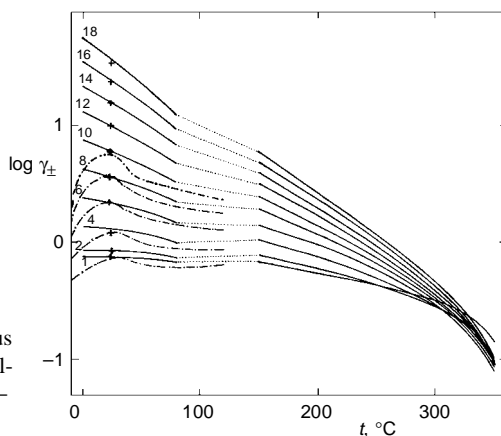


FIG. 2

Temperature dependence of $\log \gamma_{\pm}$ for various molalities of aqueous potassium hydroxide solutions: + (ref.¹¹), — (refs.^{16,17}), - - - (ref.¹⁸)

RESULTS AND DISCUSSION

The derivation of the correlation equation for $\log \gamma_{\pm} = f(m_{\text{MeOH}}, T)$ was based on the well known relations between the activity of water, a_w , in the aqueous electrolyte solution of molality m_1 and its osmotic (Φ) and mean activity coefficient γ_{\pm} (e.g. refs^{2,19}):

$$\Phi = -1\,000 \ln a_w / (M_w v_i m_1) \quad (3)$$

and

$$\ln \gamma_{\pm} = \Phi - 1 + 2 \int_0^m ((\Phi - 1)/m^{0.5}) dm^{0.5} \quad (4)$$

Here, M_w denotes the molar weight of water and v_i the total amount of ions of the given electrolyte. In the given case, $M_w = 18.01528 \text{ g mol}^{-1}$, $v_{\text{MeOH}} = 2$, so that

$$\Phi = (-27.75422/m_{\text{MeOH}}) \ln a_w = (-63.90645/m_{\text{MeOH}}) \log a_w \quad (5)$$

The following relations have been derived in a previous paper²⁰ for the molality and temperature dependence of the water activity in aqueous solutions of NaOH and KOH (using data in the above mentioned papers¹⁴⁻¹⁶):

$$\begin{aligned} \log a_{w(\text{NaOH})} = & -0.01332m + 0.002542m^2 - 3.06 \cdot 10^{-5}m^3 + \\ & + (1.5827m - 1.5669m^2 + 0.021296m^3)/T \quad (6) \end{aligned}$$

This equation is valid for $m_{\text{NaOH}} = 2-25 \text{ mol kg}^{-1}$ (i.e. 7.4-50 wt.% NaOH) and for $T = 273.15-473.15 \text{ K}$.

For KOH solutions

$$\log a_{w(\text{KOH})} = -0.02255m + 0.001434m^2 + (1.38m - 0.9254m^2)/T \quad (7)$$

valid for $m_{\text{KOH}} = 2-18 \text{ mol kg}^{-1}$ (i.e. 10-50 wt.% KOH) and for the same temperature range, 273.15-473.15 K.

Due to the validity of Eqs (6) and (7) in limited molality ranges it is necessary to transform Eq. (3) for a limited range, too:

$$\ln \gamma_{\pm} = \ln \gamma_{\pm 1} + \Phi - \Phi_1 + 2 \int_{m_1}^{m_2} ((\Phi - 1)/m^{0.5}) dm^{0.5} \quad (8)$$

or

$$\log \gamma_{\pm} = \log \gamma_{\pm 1} + (\Phi - \Phi_1)/(\ln 10) + (2/(\ln 10)) \int_{m_1}^{m_2} ((\Phi - 1)/m^{0.5}) dm^{0.5} \quad (9)$$

where $\gamma_{\pm 1}$ and Φ_1 are the known values of the mean activity and osmotic coefficients of the MeOH solution at the lower limit of the concentration range, $m_{\text{MeOH},1} = 2 \text{ mol kg}^{-1}$,

and the given temperature. Combining Eq. (5) with Eq. (6) or (7) the following relations were obtained for the concentration and temperature dependence of the osmotic coefficients:

$$\Phi_{\text{NaOH}} = 0.8512339 - 101.1447/T - (0.16245019 - 100.135/T)m + (0.001955537 - 1.360952T)m^2, \quad (10)$$

valid for $m_{\text{NaOH}} = 2\text{--}25 \text{ mol kg}^{-1}$ and $T = 273.15\text{--}473.15 \text{ K}$ and

$$\Phi_{\text{KOH}} = 1.4410904 - 88.190898T - (0.09164185 - 59.13909T)m, \quad (11)$$

valid for $m_{\text{KOH}} = 2\text{--}18 \text{ mol kg}^{-1}$ and the same temperature range, $273.15\text{--}473.15 \text{ K}$.

For the lower limit of $m_{\text{MeOH},1} = 2 \text{ mol kg}^{-1}$, Eqs (10) and (11) became simplified forms, namely

$$\Phi_{\text{NaOH},1} = 0.5341556 + 93.68149T \quad (12)$$

and

$$\Phi_{\text{KOH},1} = 1.257807 + 30.08716T. \quad (13)$$

In order to obtain the temperature dependence of the activity coefficients of NaOH or KOH solutions for the molality $m_{\text{NaOH}} = 2 \text{ mol kg}^{-1}$ in the temperature range of $273.15\text{--}473.15 \text{ K}$, it was necessary to obtain a suitable correlation equation for the temperature dependence of the mean practical activity coefficients $\gamma_{\pm,1}$ at $m_{\text{MeOH},1} = 2 \text{ mol kg}^{-1}$. This correlation was obtained by evaluating all available experimental data in refs.^{2,11–13,15,17} and in refs.^{2,11,12,14,16,17} for 2 m NaOH and 2 m KOH, respectively. The only two available experimental data at 150 and 200 °C for both kinds of solutions were supplemented by numerical interpolation for intervals of 10 K on the basis of the following relations derived now on the basis of experimental data for the range of 150–350 °C (ref.¹⁷) for 2 m NaOH solution:

$$\log \gamma_{\pm} = -82.917 + 0.68171T - 0.0020924T^2 + 2.83734E-6T^3 - 1.44E-9T^4 \quad (14)$$

and for 2 m KOH solution (see Fig. 3):

$$\log \gamma_{\pm} = -82.722 + 0.68171T - 0.0020924T^2 + 2.83734E-6T^3 - 1.44E-9T^4. \quad (15)$$

Using the least-square method the following polynomic relations were obtained on the basis of all selected available data for the temperature range $T = 273.15\text{--}473.15 \text{ K}$. For the correlation of all available experimental data the polynomial of the 6th order was used; it was therefore necessary to express all coefficients with 8–9 significant digits. Then, for 2 m NaOH solution:

$$\begin{aligned} \log \gamma_{\pm} = & 175.972176 - 2.98871232T + 0.0208479756T^2 - \\ & - 7.65562053E-5T^3 + 1.5619109E-7T^4 - \\ & - 1.68003492E-10T^5 + 7.44709291E-14T^6 \end{aligned} \quad (16)$$

and for 2 m KOH solution:

$$\begin{aligned} \log \gamma_{\pm} = & 473.494301 - 8.17278423T + 0.0581847419T^2 - \\ & - 2.18641894E-4T^3 + 4.57270983E-7T^4 - \\ & - 5.04647259E-10T^5 + 2.29069204E-13T^6 \end{aligned} \quad (17)$$

The agreement of the so calculated and experimental data of 2 m NaOH as well as 2 m KOH solutions may be held as good (see Fig. 4, where the course of the calculated values in the whole considered temperature range is depicted by full lines).

Inserting Eqs (10), (12) and (16) into Eq. (9), one obtains after integration and rearrangement, the final relation for the concentration and temperature dependence of the mean practical activity coefficient of aqueous NaOH solutions,

$$\begin{aligned} \log \gamma_{\pm, \text{NaOH}} = & 176.2940683 - 139.958399T - 2.98871232T + 0.0208479756T^2 - \\ & - 7.65562053E-5T^3 + 1.5619109E-7T^4 - 1.68003492E-10T^5 + \\ & + 7.44709291E-14T^6 - (0.141102442 - 86.97615589T)m + \\ & + (0.001273918392 - 0.886580916T)m^2 - \\ & - (0.14876612 + 101.4477T) \log m \end{aligned} \quad (18)$$

valid for $m_{\text{NaOH}} = 2-25 \text{ mol kg}^{-1}$ and $T = 273.15-473.15 \text{ K}$.

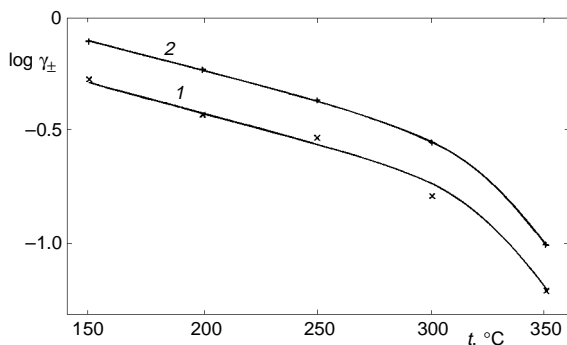


FIG. 3
Temperature dependence of $\log \gamma_{\pm}$ of 2 m NaOH (1) and KOH (2) solutions in the range 150–350 °C: after ref.¹⁷ for NaOH (x) and KOH (+); calculated from Eqs (14) and (15), respectively (—)

In a similar manner, after the insertion of Eqs (11), (13) and (17) into Eq. (9) and subsequent integration and rearrangement, the following expression for the concentration and temperature dependence of the mean practical activity coefficient of aqueous KOH solutions was obtained,

$$\begin{aligned} \log \gamma_{\pm, \text{KOH}} = & 473.5207145 - 76.18691014T - 8.17278423T + 0.05818474219T^2 - \\ & - 2.18641894E-4T^3 + 4.57270983E-7T^4 - 5.04647259E-10T^5 + \\ & + 2.29609204E-13T^6 - (0.0795991 - 51.36750792T)m + \\ & + (0.4410904 - 88.190898T) \log m, \end{aligned} \quad (19)$$

valid for $m_{\text{KOH}} = 2\text{--}18 \text{ mol kg}^{-1}$ and $T = 273.15\text{--}473.15 \text{ K}$.

A comparison of the so calculated values of decadic logarithms of the mean molal activity coefficients with experimental data for NaOH solutions according to refs^{11,15,17} and KOH solutions according to refs^{11,16,17} is given in Tables I and II. As may be seen, quite good agreement between both kinds of values may be observed for KOH solutions at almost the whole considered range of molalities and temperatures, while for NaOH solutions the deviations are somewhat more evident at temperatures lower than 25 °C. With respect to the numerical scatter of experimental results of various authors (see e.g. Figs 1–4), the obtained relations (18) and (19) can therefore be considered as sufficiently reliable for the calculation of the mean activity coefficients of aqueous NaOH and KOH solutions in dependence on their concentration in the range $m_{\text{NaOH}} = 2\text{--}25$ and $m_{\text{KOH}} = 2\text{--}18 \text{ mol kg}^{-1}$ and temperature range 0–200 °C. In addition, calculated data represent suitable continuous supplementation of lacking experimental data in the temperature range 70 or 80 and 150 °C. They may find a good application especially for solving various equilibrium problems in technically important systems containing

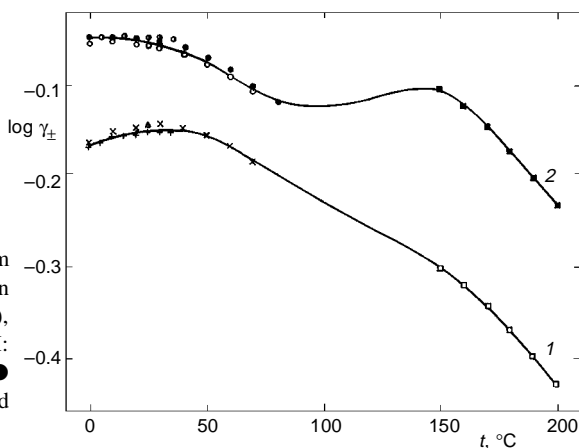


FIG. 4

Temperature dependence of $\log \gamma_{\pm}$ of 2 m NaOH (1) and KOH (2) solutions in the range 0–200 °C; NaOH: Δ (ref.¹¹), $+$ (ref.¹³), \times (ref.¹⁵), \square (ref.¹⁷); KOH: \circ (ref.²), \blacktriangle (ref.¹¹), \circ (ref.¹⁴), \bullet (ref.¹⁶), \blacksquare (ref.¹⁷); — calculated from Eqs (16) and (17), respectively

TABLE I

Calculated (upper data, Eq. (18)) and experimental values (lower data, 0–70 °C (ref.¹⁵), 25 °C (ref.¹¹), 150–200 °C (ref.¹⁷)) of $\log \gamma_{\pm}$ of aqueous NaOH solutions in the range of $m_{\text{NaOH}} = 2\text{--}24 \text{ mol kg}^{-1}$ and temperature $t = 0\text{--}200 \text{ }^{\circ}\text{C}$

$t, \text{ }^{\circ}\text{C}$	$m_{\text{NaOH}}, \text{ mol kg}^{-1}$											
	2	4	6	8	10	12	14	16	18	20	22	24
0	-0.1685	+0.0058	0.2294	0.4639	0.6971	0.9238	1.1411	1.3472	1.5412	1.7221	1.8896	2.0432
	-0.1664	-0.0458	0.1438	0.3718	0.6153	0.8547	1.0553	1.2528	1.4502	-	-	-
10	-0.1613	-0.0041	0.2017	0.4185	0.6346	0.8449	1.0465	1.2378	1.4177	1.5855	1.7407	1.8828
	-0.1539	-0.0360	0.1451	0.3646	0.5994	0.8242	1.0003	1.1858	1.3713	-	-	-
20	-0.1514	-0.0139	0.1751	0.3755	0.5757	0.7707	0.9577	1.1352	1.3021	1.4575	1.6012	1.7327
	-0.1495	-0.0382	0.1309	0.3372	0.5578	0.7633	0.9388	1.1125	1.2861	-	-	-
25	-0.1533	-0.0197	0.1614	0.3540	0.5466	0.7344	0.9145	1.0854	1.2460	1.3957	1.5339	1.6603
	-0.1464	-0.0403	0.1147	0.3050	0.5130	0.7194	0.9076	1.0664	1.1922	1.2881	1.3622	1.4236
30	-0.1526	-0.0263	0.1472	0.3322	0.5175	0.6982	0.8717	1.0362	1.1908	1.3349	1.4678	1.5893
	-0.1475	-0.0406	0.1189	0.3134	0.5205	0.7085	0.8710	1.0329	1.1947	-	-	-
40	-0.1545	-0.0422	0.1167	0.2873	0.4587	0.6261	0.7867	0.9392	1.0824	1.2157	1.3386	1.4508
	-0.1503	-0.0479	0.1028	0.2847	0.4765	0.6469	0.7967	0.9469	1.0970	-	-	-
50	-0.1609	-0.0617	0.0835	0.2407	0.3990	0.5538	0.7025	0.8436	0.9761	1.0993	1.2128	1.3162
	-0.1573	-0.0594	0.0828	0.2517	0.4266	0.5786	0.7161	0.8546	0.9930	-	-	-
60	-0.1710	-0.0842	0.0482	0.1927	0.3387	0.4817	0.6192	0.7496	0.8720	0.9858	1.0904	1.1856
	-0.1695	-0.0760	0.0582	0.2133	0.3699	0.5036	0.6292	0.7560	0.8829	-	-	-

TABLE I
(Continued)

$t, ^\circ\text{C}$	$m_{\text{NaOH}}, \text{mol kg}^{-1}$											
	2	4	6	8	10	12	14	16	18	20	22	24
70	-0.1839	-0.1086	0.0116	0.1442	0.2787	0.4106	0.5374	0.6578	0.7707	0.8756	0.9719	1.0593
	-0.1858	-0.0969	0.0298	0.1708	0.3075	0.4226	0.5358	0.6511	0.7664	-	-	-
80	-0.1983	-0.1340	-0.0252	0.0961	0.2197	0.3412	0.4580	0.5689	0.6729	0.7693	0.8578	0.9379
	-	-	-	-	-	-	-	-	-	-	-	-
90	-0.2132	-0.1593	-0.0613	0.0494	0.1627	0.2742	0.3816	0.4836	0.5791	0.6676	0.7486	0.8218
	-	-	-	-	-	-	-	-	-	-	-	-
100	-0.2280	-0.1839	-0.0960	0.0045	0.1081	0.2102	0.3087	0.4022	0.4897	0.5707	0.6447	0.7114
	-	-	-	-	-	-	-	-	-	-	-	-
110	-0.2422	-0.2073	-0.1292	-0.0382	0.0561	0.1494	0.2395	0.3249	0.4048	0.4787	0.5460	0.6065
	-	-	-	-	-	-	-	-	-	-	-	-
120	-0.2558	-0.2298	-0.1608	-0.0788	0.0067	0.0916	0.1736	0.2514	0.3241	0.3912	0.4522	0.5068
	-	-	-	-	-	-	-	-	-	-	-	-
130	-0.2692	-0.2516	-0.1913	-0.1180	-0.0408	0.0361	0.1104	0.1810	0.2469	0.3075	0.3625	0.4115
	-	-	-	-	-	-	-	-	-	-	-	-

TABLE I
(Continued)

$t, ^\circ\text{C}$	$m_{\text{NaOH}}, \text{mol kg}^{-1}$											
	2	4	6	8	10	12	14	16	18	20	22	24
140	-0.2832	-0.2735	-0.2216	-0.1564	-0.0872	-0.0179	0.0492	0.1128	0.1722	0.2267	0.2760	0.3197
150	-0.2987	-0.2963	-0.2526	-0.1952	-0.1336	-0.0716	-0.0114	0.0457	0.0988	0.1475	0.1913	0.2300
	-0.227	-0.253	-0.213	-0.164	-0.112	-0.056	0.000	0.055	0.110	0.157	0.197	0.230
160	-0.3167	-0.3219	-0.2854	-0.2355	-0.1810	-0.1260	-0.0724	-0.0216	0.0257	0.0688	0.1074	0.1412
170	-0.3380	-0.3501	-0.3208	-0.2780	-0.2304	-0.1820	-0.1347	-0.0899	-0.0483	0.0105	0.0232	0.0524
180	-0.3628	-0.3815	-0.3591	-0.3231	-0.2822	-0.2400	-0.1988	-0.1597	-0.1235	-0.0908	-0.0618	-0.0371
190	-0.3908	-0.4159	-0.4000	-0.3705	-0.3359	-0.2998	-0.2643	-0.2307	-0.1997	-0.1718	-0.1474	-0.1268
200	-0.4202	-0.4513	-0.4418	-0.4186	-0.3899	-0.3596	-0.3297	-0.3013	-0.2752	-0.2520	-0.2320	-0.2154
	-0.431	-0.450	-0.440	-0.422	-0.398	-0.371	-0.345	-0.319	-0.292	-0.270	-0.250	-0.228

TABLE II

Calculated (upper data, Eq. (19)) and experimental values (lower data, 0–70 °C (ref.¹⁶), 25 °C (ref.¹¹), 150–200 °C (ref.¹⁷)) of $\log \gamma_{\pm}$ of aqueous KOH solutions in the range of $m_{\text{KOH}} = 2\text{--}18 \text{ mol kg}^{-1}$ and temperature $t = 0\text{--}200 \text{ }^{\circ}\text{C}$

$t, \text{ }^{\circ}\text{C}$	$m_{\text{KOH}}, \text{ mol kg}^{-1}$									
	2	4	6	8	10	12	14	16	18	
0	-0.0532	0.1993	0.4371	0.6688	0.8971	1.1234	1.3482	1.5720	1.7950	
	-0.0590	0.1422	0.3846	0.6401	0.8923	1.1316	1.3550	1.5657	1.7728	
10	-0.0550	0.1876	0.4141	0.6339	0.8501	1.0640	1.2763	1.4874	1.6977	
	-0.0576	0.1394	0.3727	0.6167	0.8569	1.0849	1.2982	1.4998	1.6981	
20	-0.0558	0.1777	0.3937	0.6024	0.8073	1.0096	1.2103	1.4097	1.6081	
	-0.0596	0.1320	0.3560	0.5891	0.8180	1.0354	1.2392	1.4322	1.6219	
25	-0.0573	0.1719	0.3828	0.5863	0.7858	0.9827	1.1778	1.3716	1.5644	
	-0.0656	0.1242	0.3389	0.5625	0.7860	1.0021	1.2043	1.3863	1.5422	
30	-0.0599	0.1650	0.3711	0.5696	0.7638	0.9554	1.1452	1.3336	1.5209	
	-0.0646	0.1204	0.3351	0.5576	0.7759	0.9835	1.1784	1.3629	1.5437	
40	-0.0687	0.1481	0.3451	0.5339	0.7182	0.8997	1.0793	1.2574	1.4344	
	-0.0728	0.1046	0.3097	0.5220	0.7305	0.9290	1.1153	1.2913	1.4624	
50	-0.0814	0.1280	0.3163	0.4960	0.6711	0.8431	1.0131	1.1815	1.3489	
	-0.0833	0.0855	0.2808	0.4834	0.6827	0.8726	1.0508	1.2180	1.3783	

TABLE II
(Continued)

$t, ^\circ\text{C}$	$m_{\text{KOH}}, \text{mol kg}^{-1}$								
	2	4	6	8	10	12	14	16	18
60	-0.0958	0.1065	0.2868	0.4580	0.6242	0.7874	0.9484	1.1078	1.2660
	-0.0968	0.0624	0.2478	0.4409	0.6316	0.8136	0.9839	1.1419	1.2896
70	-0.1094	0.0862	0.2588	0.4220	0.5800	0.7348	0.8873	1.0382	1.1878
	-0.1120	0.0368	0.2121	0.3960	0.5787	0.7535	0.9161	1.0642	1.1973
80	-0.1201	0.0693	0.2345	0.3903	0.5405	0.6874	0.8319	0.9747	1.1162
	-	-	-	-	-	-	-	-	-
90	-0.1263	0.0572	0.2158	0.3642	0.5071	0.6465	0.7835	0.9187	1.0526
	-	-	-	-	-	-	-	-	-
100	-0.1273	0.0542	0.2026	0.3443	0.4803	0.6126	0.7424	0.8704	0.9970
	-	-	-	-	-	-	-	-	-
110	-0.1240	0.0485	0.1945	0.3298	0.4592	0.5848	0.7079	0.8290	0.9488
	-	-	-	-	-	-	-	-	-
120	-0.1179	0.0495	0.1898	0.3190	0.4421	0.5614	0.6780	0.7927	0.9059
	-	-	-	-	-	-	-	-	-

TABLE II
(Continued)

$t, ^\circ\text{C}$	$m_{\text{KOH}}, \text{mol kg}^{-1}$								
	2	4	6	8	10	12	14	16	18
130	-0.1116	0.0510	0.1858	0.3092	0.4264	0.5396	0.6501	0.7587	0.8657
140	-0.1083	0.0497	0.1793	0.2972	0.4087	0.5162	0.6209	0.7236	0.8247
150	-0.1111	0.0426	0.1671	0.2798	0.3859	0.4879	0.5871	0.6842	0.7797
	-0.107	0.025	0.155	0.288	0.400	0.510	0.604	0.699	0.780
160	-0.1226	0.0269	0.1467	0.2544	0.3554	0.4522	0.5460	0.6378	0.7279
170	-0.1436	0.0019	0.1171	0.2200	0.3161	0.4079	0.4967	0.5834	0.6684
180	-0.1728	-0.0310	0.0799	0.1782	0.2696	0.3566	0.4406	0.5224	0.6026
190	-0.2046	-0.0665	0.0403	0.1342	0.2212	0.3036	0.3830	0.4602	0.5356
200	-0.2286	-0.0940	0.0088	0.0985	0.1811	0.2592	0.3342	0.4069	0.4779
	-0.230	-0.123	-0.020	0.073	0.152	0.232	0.306	0.386	0.455

aqueous NaOH or KOH solutions under the given reaction conditions. For the most exact calculations it is evidently necessary to use new values of this quantity which are to be determined with the use of an exact as possible method within the whole range of the reaction conditions.

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